

# HEAT TRANSFER

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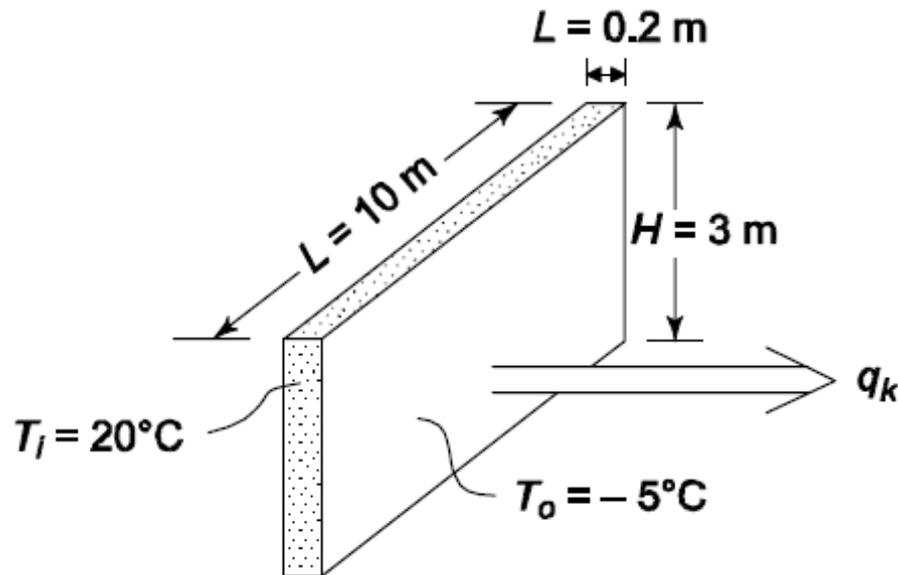
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# Problems

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## Problem 1

If inner and outer faces of a concrete wall with thickness of 20 cm is kept at a temperature  $20^{\circ}\text{C}$  and  $-5^{\circ}\text{C}$ , respectively, and the thermal conductivity of the concrete is  $1.2\text{ W/m.K}$ . Determine the heat loss through a wall 10 m long and 3 m high.

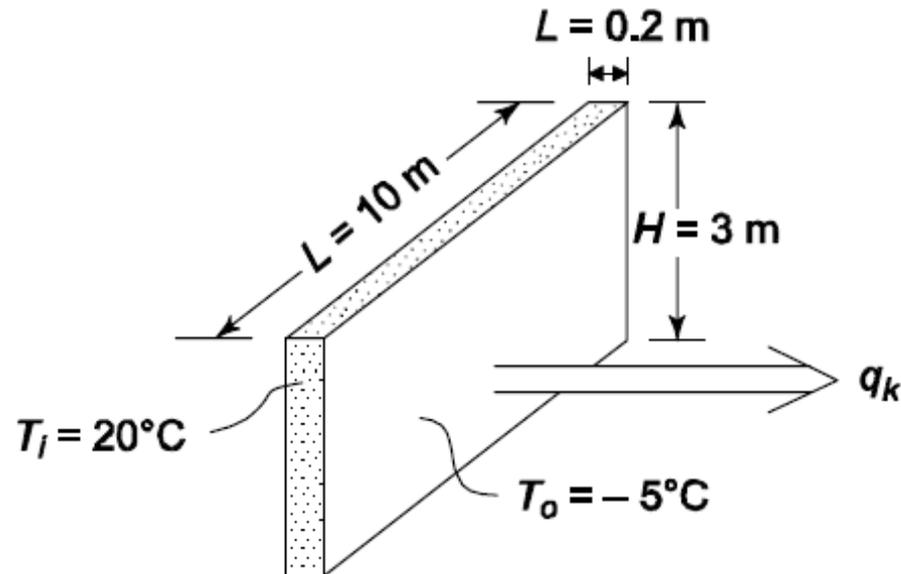


# Problems

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## Problem 1

- 10 m long, 3 m high, and 0.2 m thick concrete wall.
- Thermal conductivity of the concrete ( $k$ ) = 1.2 W/m.K
- Temperature of the inner surface ( $T_i$ ) = 20 °C
- Temperature of the outer surface ( $T_o$ ) = -5 °C
- One dimensional heat flow
- The system has reached steady state.



# Problems

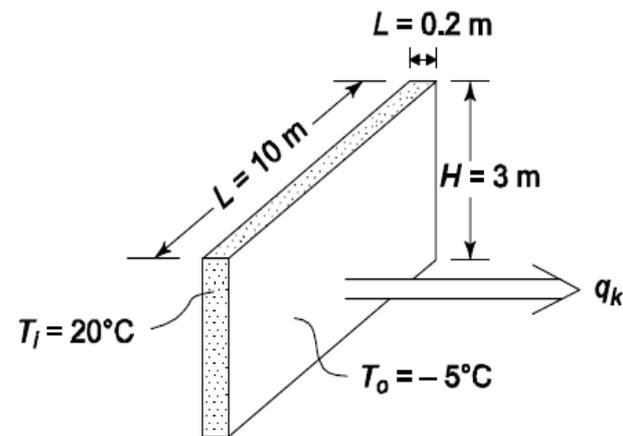
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## Problem 1

$$q = \frac{AK}{L} (\Delta T)$$

$$q = \frac{(10\text{ m})(3\text{ m})(1.2\text{ W}/(\text{m K}))}{0.2\text{ m}} (20^\circ\text{C} - (-5^\circ\text{C}))$$

$$q = 4500\text{ W}$$

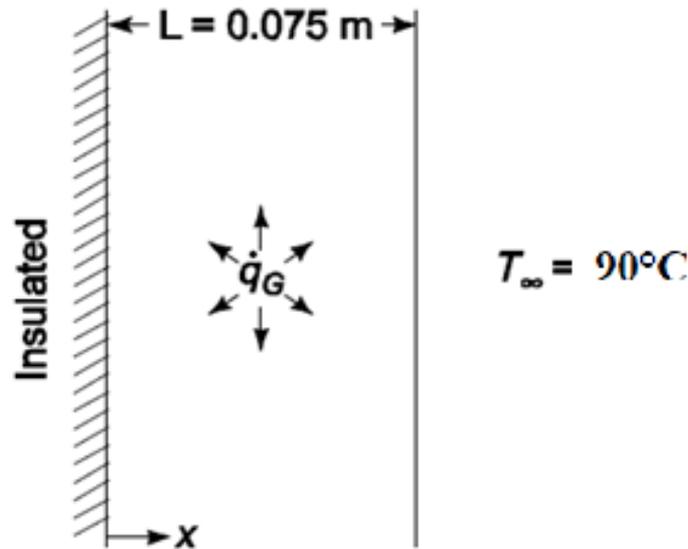


# Problems

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## Problem 2

A wall with 7.5 cm thickness (shown below) generates heat at the rate of  $105 \text{ W/m}^3$ . One side of the wall is insulated, and the other side is exposed to an environment at  $90^\circ\text{C}$ . The convective heat transfer coefficient between the wall and the environment is  $500 \text{ W/m}^2\cdot\text{K}$ . Under one-dimensional-steady state conditions, and if the thermal conductivity of the wall is  $12 \text{ W/m}\cdot\text{K}$ , calculate the maximum temperature in the wall.

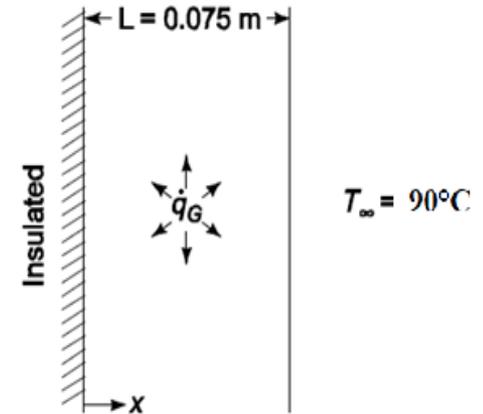


# Problems

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## Problem 2

- Plane wall with internal heat generation
- Thickness ( $L$ ) = 0.075 m
- Internal heat generation rate ( $q_G$ ) = 105 W/m<sup>3</sup>
- One side is insulated
- Ambient temperature on the other side ( $T$ ) = 90 °C
- Convective heat transfer coefficient ( $h_c$ ) = 500 W/(m<sup>2</sup> K)
- Thermal conductivity ( $k$ ) = 12 W/m.K.
- The heat loss through the insulation is negligible.
- The system has reached steady state.
- One dimensional conduction through the wall.



# Problems

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## Problem 2

The one dimensional conduction equation:

$$k \frac{\partial^2 T}{\partial x^2} + \dot{q}_G = \rho c \frac{\partial T}{\partial t}$$

For steady state,  $\frac{\partial T}{\partial t} = 0$  therefore

$$k \frac{d^2 T}{dx^2} + \dot{q}_G = 0$$

$$\frac{d^2 T}{dx^2} = - \frac{\dot{q}_G}{k}$$

To solve this equation, two boundary conditions are needed:

1. No energy loss through the insulator.
2. Convection at the other surface

# Problems

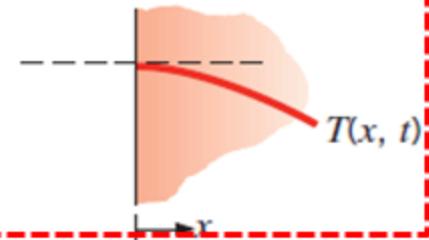
## Problem 2

1. No energy loss through the insulator.

*Insulated surface*

Adiabatic or insulated surface

$$\left. \frac{\partial T}{\partial x} \right|_{x=0} = 0 \quad (2.33)$$

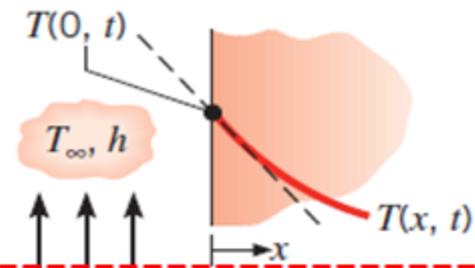


2. Convection at the other surface

*Fluid flow near to  
the surface*

Convection surface condition

$$-k \left. \frac{\partial T}{\partial x} \right|_{x=0} = h[T_\infty - T(0, t)] \quad (2.34)$$



# Problems

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## Problem 2

1. No energy loss through the insulator.

$$\frac{d^2 T}{dx^2} = -\frac{\dot{q}_G}{k} \quad \Rightarrow \quad \frac{dT}{dx} = \frac{\dot{q}_G}{k} x + C_1$$
$$\frac{dT}{dx} = 0 \text{ at } x = 0$$
$$0 = -\frac{\dot{q}_G}{k} (0) + C_1 \Rightarrow C_1 = 0$$

Integrating again

$$T = -\frac{\dot{q}_G}{2k} x^2 + C_2$$

# Problems

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## Problem 2

2. Convection at the other surface

$$T = -\frac{\dot{q}_G}{2k} x^2 + C_2$$

$$-k \frac{dT}{dx} = h_c (T - T_\infty) \quad \text{at } x = L$$

$$-k \left( \frac{\dot{q}_G L}{k} \right) = h_c \left( -\frac{\dot{q}_G L^2}{2k} + C_2 - T_\infty \right) \Rightarrow C_2 = \dot{q}_G L \left( \frac{1}{h_c} + \frac{L}{2k} \right) + T_\infty$$

# Problems

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## Problem 2

Substituting this into the expression for  $T$  yields the temperature distribution in the wall:

$$T(x) = \frac{\dot{q}_G}{2k} x^2 + \dot{q}_G L \left( \frac{1}{h_c} + \frac{L}{2k} \right) + T_\infty$$

$$T(x) = T_\infty + \frac{\dot{q}_G}{2k} \left( L^2 + \frac{2kL}{h_c} - x^2 \right)$$

The maximum temperature occurs at  $x = 0$ .

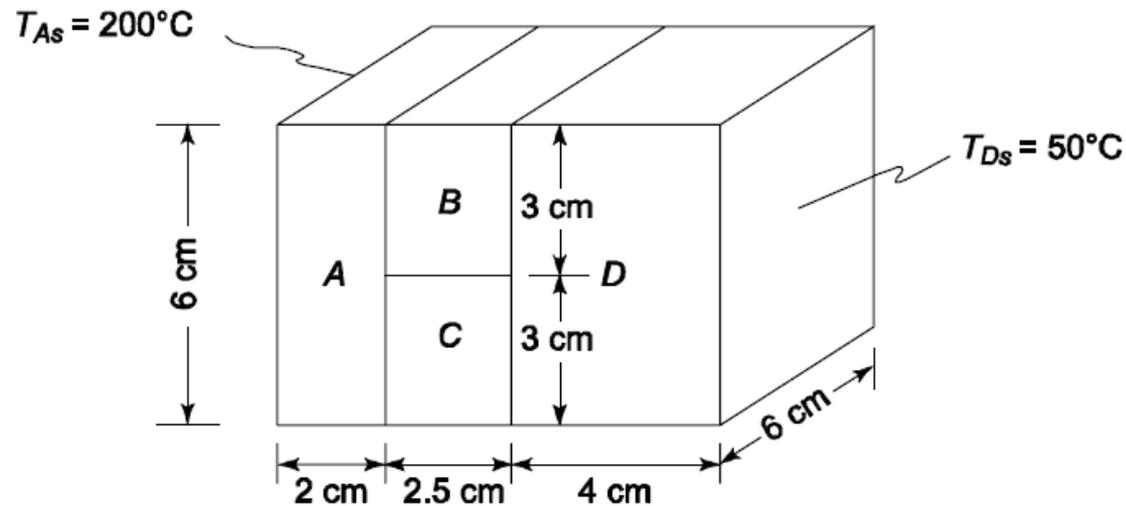
$$T_{\max} = T_\infty + \frac{\dot{q}_G}{2k} \left( L^2 + \frac{2kL}{h_c} \right)$$

$$T_{\max} = 90^\circ\text{C} + \frac{10^5 \text{ W/m}^3}{2[12 \text{ W/(mK)}]} \left( (0.075 \text{ m})^2 + \frac{2[12 \text{ W/(mK)}](0.075 \text{ m})}{500 \text{ W/(m}^2\text{K)}} \right) = 128^\circ\text{C}$$

# Problems

## Problem 3

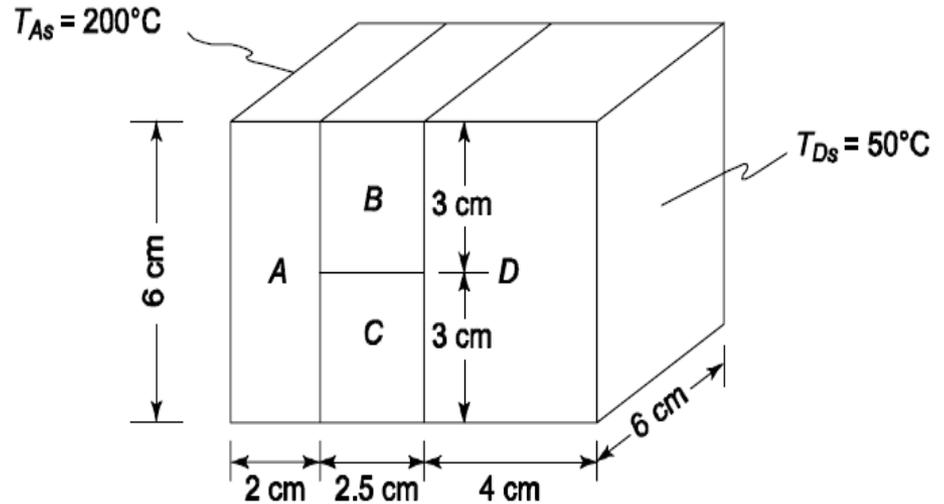
A composite wall (shown below) has uniform temperatures. If the thermal conductivities of the wall materials are:  $k_A = 70 \text{ W/m.K}$ ,  $k_B = 60 \text{ W/m.K}$ ,  $k_C = 40 \text{ W/m.K}$ , and  $k_D = 20 \text{ W/m.K}$ , determine the rate of heat transfer through this section of the wall and the temperatures at the interfaces. (Surfaces normal to heat transfer direction are isothermal).



# Problems

## Problem 3

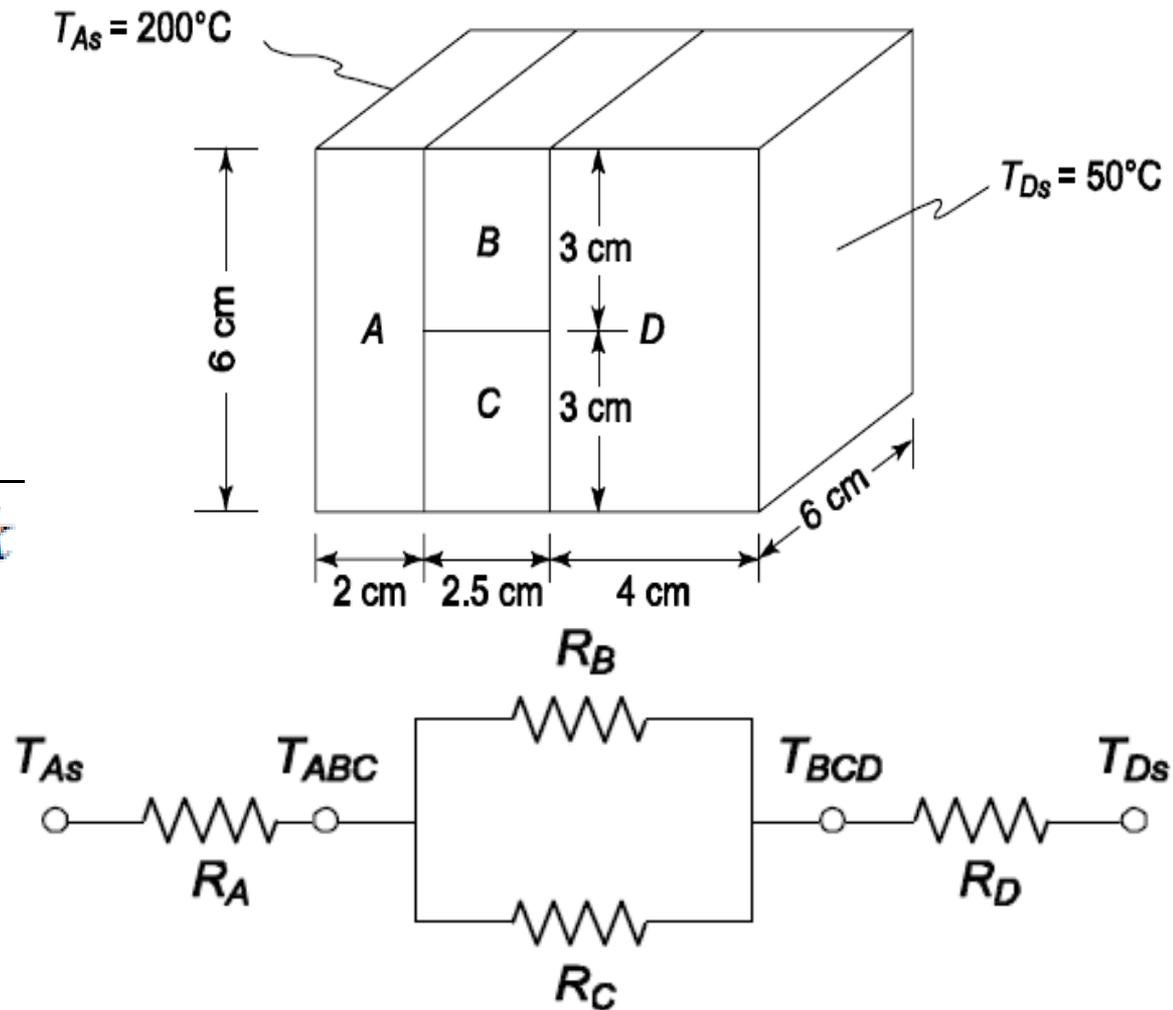
- A section of a composite wall
- Thermal conductivities
- $k_A = 70 \text{ W/m.K}$
- $k_B = 60 \text{ W/m.K}$
- $k_C = 40 \text{ W/m.K}$
- $k_D = 20 \text{ W/m.K}$
- Surface temperatures
- Left side ( $T_{As}$ ) =  $200 \text{ }^\circ\text{C}$
- Right side ( $T_{Ds}$ ) =  $50 \text{ }^\circ\text{C}$
- One dimensional conduction
- The system is in steady state
- The contact resistances between the materials is negligible



# Problems

## Problem 3

$$R_k = \frac{L}{Ak}$$



# Problems

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## Problem 3

The total thermal resistance is

$$R_{\text{total}} = R_A + \frac{R_B R_C}{R_B + R_C} + R_D$$

$$R_{\text{total}} = 0.0794 + \frac{(0.2315)(0.3472)}{0.2315 + 0.3472} + 0.5556 \text{ K/W}$$

$$R_{\text{total}} = 0.7738 \text{ K/W}$$

The total rate of heat transfer through the composite wall is given by

$$q = \frac{\Delta T}{R_{\text{total}}} = \frac{200^\circ\text{C} - 50^\circ\text{C}}{0.7738 \text{ K/W}} = 194 \text{ W}$$

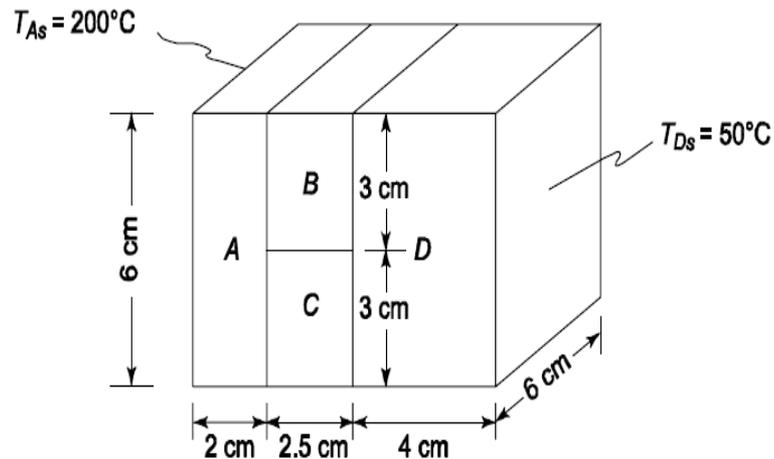
# Problems

## Problem 3

The average temperature at the interface between material *A* and materials *B* and *C* ( $T_{ABC}$ ) can be determined by considering the conduction through material *A* alone.

$$q_{ka} = \frac{T_{As} - T_{ABC}}{R_A} = q$$

$$T_{ABC} = T_{As} - q R_A = 200^\circ\text{C} - (194 \text{ W}) (0.0794 \text{ K/W}) = 185^\circ\text{C}$$



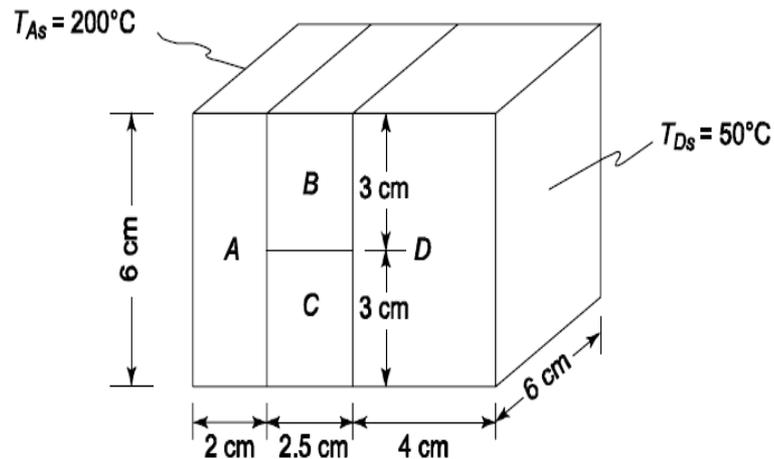
# Problems

## Problem 3

The average temperature at the interface between material  $D$  and materials  $B$  and  $C$  ( $T_{BCD}$ ) can be determined by considering the conduction through material  $D$  alone

$$q_{kD} = \frac{T_{BCD} - T_{Ds}}{R_D} = q$$

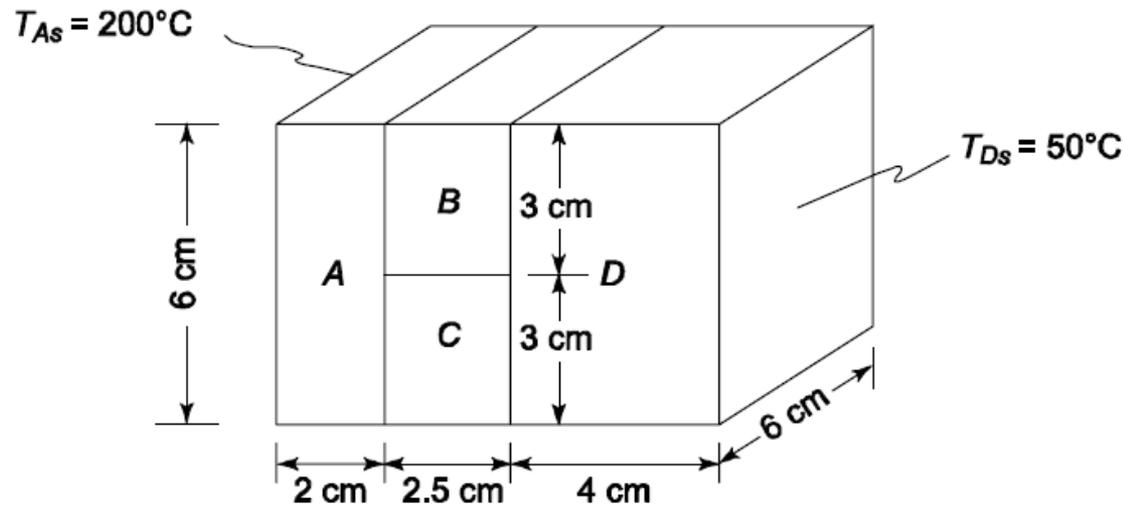
$$T_{BCD} = T_{Ds} + q R_D = 50^\circ\text{C} + (194 \text{ W}) (0.5556 \text{ K/W}) = 158^\circ\text{C}$$



# Problems

## Problem 4

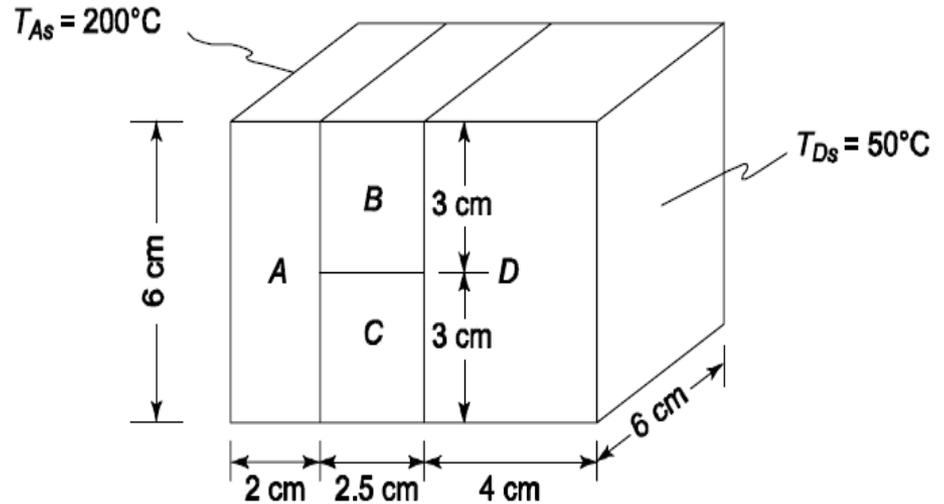
A composite wall (shown below) has uniform temperatures. If the thermal conductivities of the wall materials are:  $k_A = 70 \text{ W/m.K}$ ,  $k_B = 60 \text{ W/m.K}$ ,  $k_C = 40 \text{ W/m.K}$ , and  $k_D = 20 \text{ W/m.K}$ , **and contact resistance at each interface  $R_i = 0.1 \text{ K/W}$** , determine the rate of heat transfer through this section of the wall and the temperatures at the interfaces. (Surfaces normal to heat transfer direction are isothermal).



# Problems

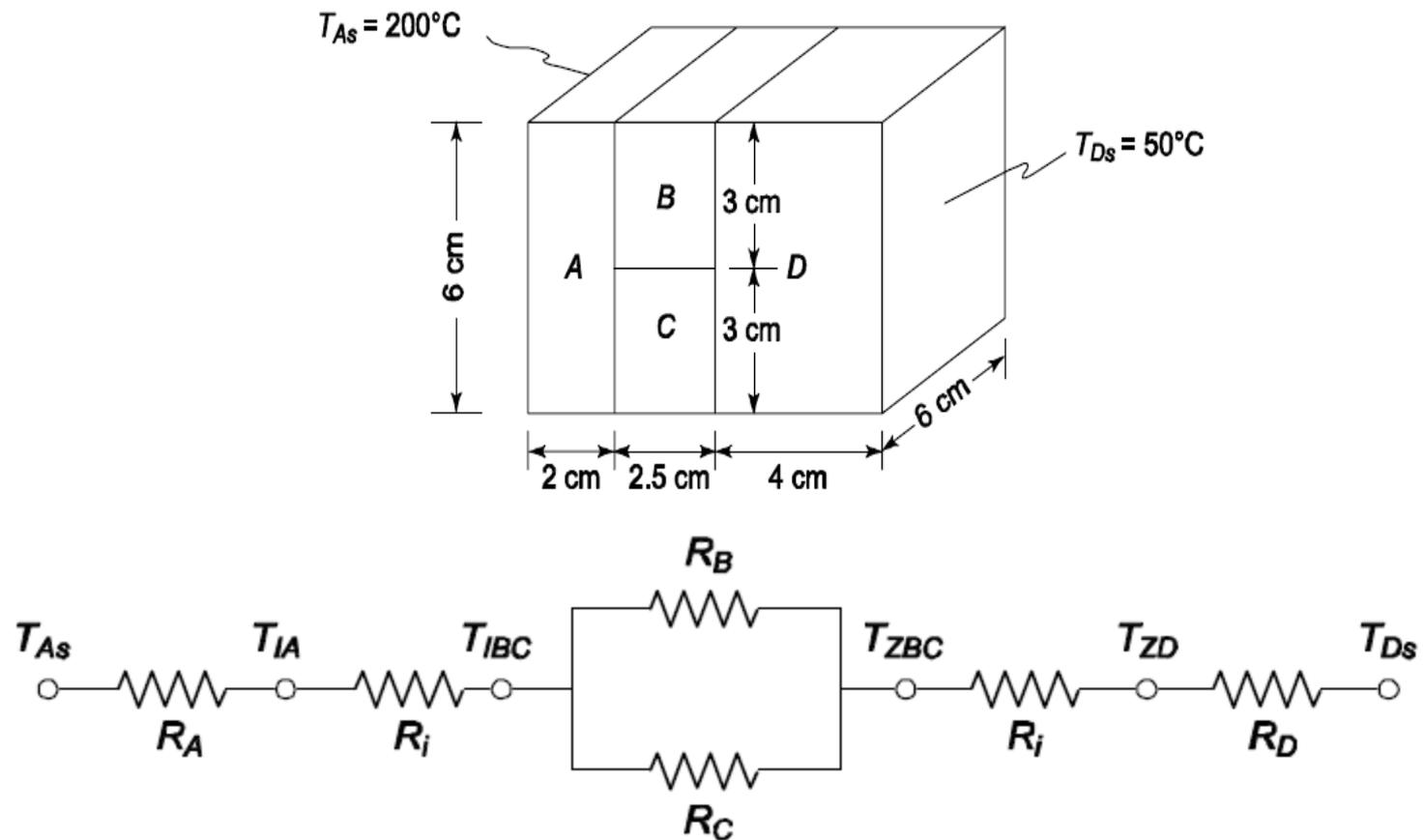
## Problem 4

- A section of a composite wall
- Thermal conductivities
- $k_A = 70 \text{ W/m.K}$
- $k_B = 60 \text{ W/m.K}$
- $k_C = 40 \text{ W/m.K}$
- $k_D = 20 \text{ W/m.K}$
- Surface temperatures
- Left side ( $T_{As}$ ) =  $200 \text{ }^\circ\text{C}$
- Right side ( $T_{Ds}$ ) =  $50 \text{ }^\circ\text{C}$
- One dimensional conduction
- The system is in steady state
- **Contact resistance at each interface ( $R_i$ ) =  $0.1 \text{ K/W}$**



# Problems

## Problem 4



# Problems

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## Problem 4

(a) The total resistance for this system is

$$R_{\text{total}} = R_A + R_i + \frac{R_B R_C}{R_B + R_C} + R_i + R_D$$

$$R_{\text{total}} = 0.0794 + 0.1 + \frac{(0.2315)(0.3472)}{0.2315 + 0.3472} + 0.1 + 0.5556 \text{ K/W}$$

$$R_{\text{total}} = 0.9738 \text{ K/W}$$

The total rate of heat transfer through the composite wall is given by:

$$q = \frac{\Delta T}{R_{\text{total}}} = \frac{200^\circ\text{C} - 50^\circ\text{C}}{0.9738 \text{ K/W}} = 154 \text{ W}$$

# Problems

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## Problem 4

(b) The average temperature on the *A* side of the interface between material *A* and material *B* and *C* ( $T_{1A}$ ) can be determined by **considering the conduction through material *A* alone.**

$$q = \frac{T_{As} - T_{1A}}{R_A}$$

$$T_{1A} = T_{As} - q R_A = 200^\circ\text{C} - (154 \text{ W}) (0.0794 \text{ K/W}) = 188^\circ\text{C}$$

The average temperature on the *B* and *C* side of the interface between material *A* and materials *B* and *C* ( $T_{1BC}$ ) can be determined by **considering the heat transfer through the contact resistance.**

$$q = \frac{T_{1A} - T_{1BC}}{R_i}$$

$$T_{1BC} = T_{1A} - q R_i = 188^\circ\text{C} - (154 \text{ W}) (0.1 \text{ K/W}) = 172^\circ\text{C}$$

# Problems

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## Problem 4

The average temperature on the  $D$  side of the interface between material  $D$  and materials  $B$  and  $C$  ( $T_{2D}$ ) can be determined by **considering the conduction through material  $D$  alone.**

$$q = \frac{T_{2D} - T_{Ds}}{R_D}$$

$$T_{2D} = T_{Ds} + q R_D = 50^\circ\text{C} + (154 \text{ W}) (0.5556 \text{ K/W}) = 136^\circ\text{C}$$

The average temperature on the  $B$  and  $C$  side of the interface between material  $D$  and materials  $B$  and  $C$  ( $T_{2BC}$ ) can be determined by **considering the heat transfer through the contact resistance.**

$$q = \frac{T_{2BC} - T_{2D}}{R_i}$$

$$T_{2BC} = T_{2D} + q R_i = 136^\circ\text{C} + (154 \text{ W}) (0.1 \text{ K/W}) = 151^\circ\text{C}$$